

## Chapter 2

### Short Answer Problems

- The LMTD factor is required for heat exchangers when the two streams do not exhibit pure counter-current flow. Most exchangers such as S&T and other arrangements fall into this category.
- This statement is not generally true. In fact, condensers often have high heat transfer coefficients on the condensing side. One exception is for partial condensers where the majority of the condenser-side of the exchanger comprises of non-condensing gas – in this case the heat transfer coefficient on the condensing side may be limiting.
- Turbulent flow on both sides of the heat exchanger – see Table 2.9
  - Shell-side  $h \propto Re^{0.6}$   $\frac{h}{h_{\text{base}}} = \frac{1.5^{0.6}}{1}$  1.275 or and increase of 27.5%
  - Tube-side  $h \propto Re^{0.8}$   $\frac{h}{h_{\text{base}}} = \frac{1.5^{0.8}}{1}$  1.383 or and increase of 38.3%
- Laminar flow on both sides of the heat exchanger – see Table 2.9
  - Shell-side  $h \propto Re^{0.45}$   $\frac{h}{h_{\text{base}}} = \frac{1.5^{0.45}}{1}$  1.20 or and increase of 20%
  - Tube-side  $h \propto Re^{0.3}$   $\frac{h}{h_{\text{base}}} = \frac{1.5^{0.3}}{1}$  1.145 or and increase of 14.5%
- All else considered, the heat transfer coefficient for turbulent flow will be (much) higher than for laminar flow. For this reason when possible flow should be in the turbulent regime.
- Refer to Section 2.2.1.7 – three reasons for placing a fluid on the tube side of a S&T exchanger
  - 2-If the fluid is corrosive
  - 2-If the fluid causes severe fouling or scaling
  - 2-If the fluid is at a much higher pressure than the other fluid
  - 2-If the fluid has a much higher film coefficient
  - 2-If the material in contact with the fluid must be an expensive alloy

# Conceptual Design Of Chemical Process Solution Manual

**Xiaolong Qi**



## **Conceptual Design Of Chemical Process Solution Manual:**

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